

Subcooled Convective Boiling in Structured Surface Microchannels

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Items



Abstract

Test Section and Flow Loop

Experimental Results

1. Effect of geometry and flow parameter on CHF
2. Boiling curve/ two phase heat transfer coefficient
3. Bubble ebullition cycle
4. Flow pattern and morphology
5. Enhancement performance ratio
6. Comparison with existing data

Conclusions

Salient References

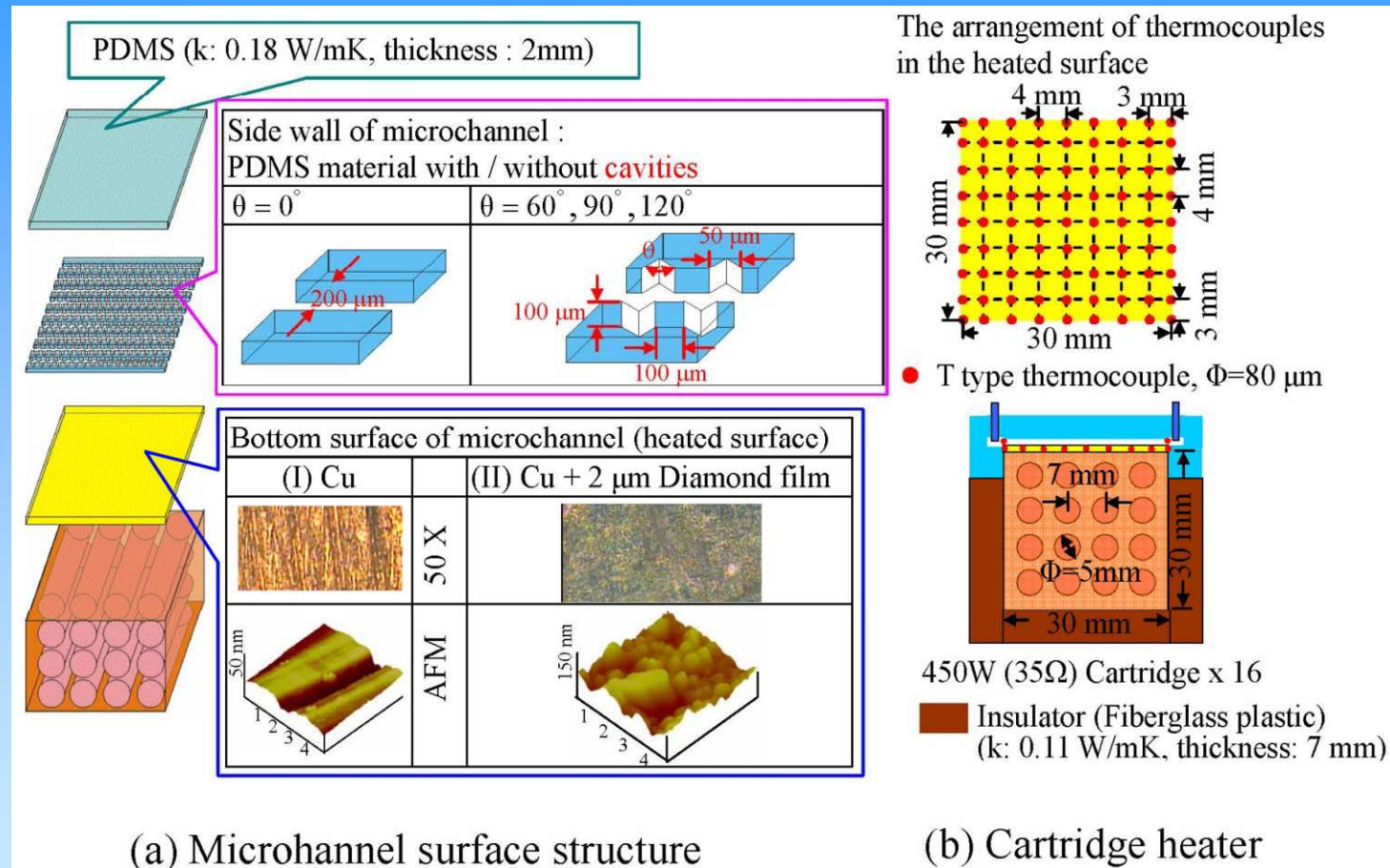
Abstract



Experiments are performed to investigate *subcooled flow boiling* of *DI water* and *FC-72* in parallel microchannels, and try to rise the critical heat flux (CHF) and heat transfer coefficient to enhance the cooling efficiency. Three major methods were used in this study below:

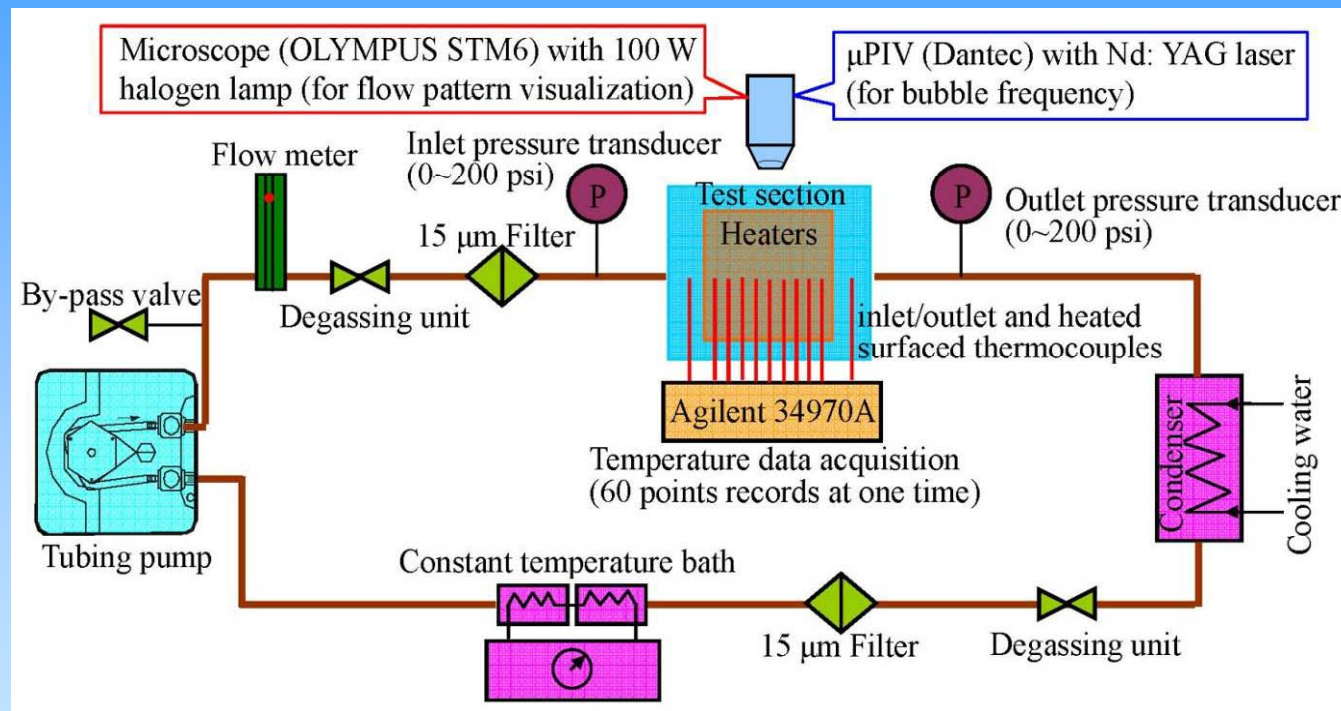
1. To add the *cavity angle* of $\theta = 60^\circ$, 90° , and 120° on the microchannel side walls.
2. To coat *2 μm diamond film* in the Cu heated surface.
3. To add *1 vol. %* Multi-walled Carbon Nanotube (*MCNT*) into the working medium (de-ionized water).

Test Section



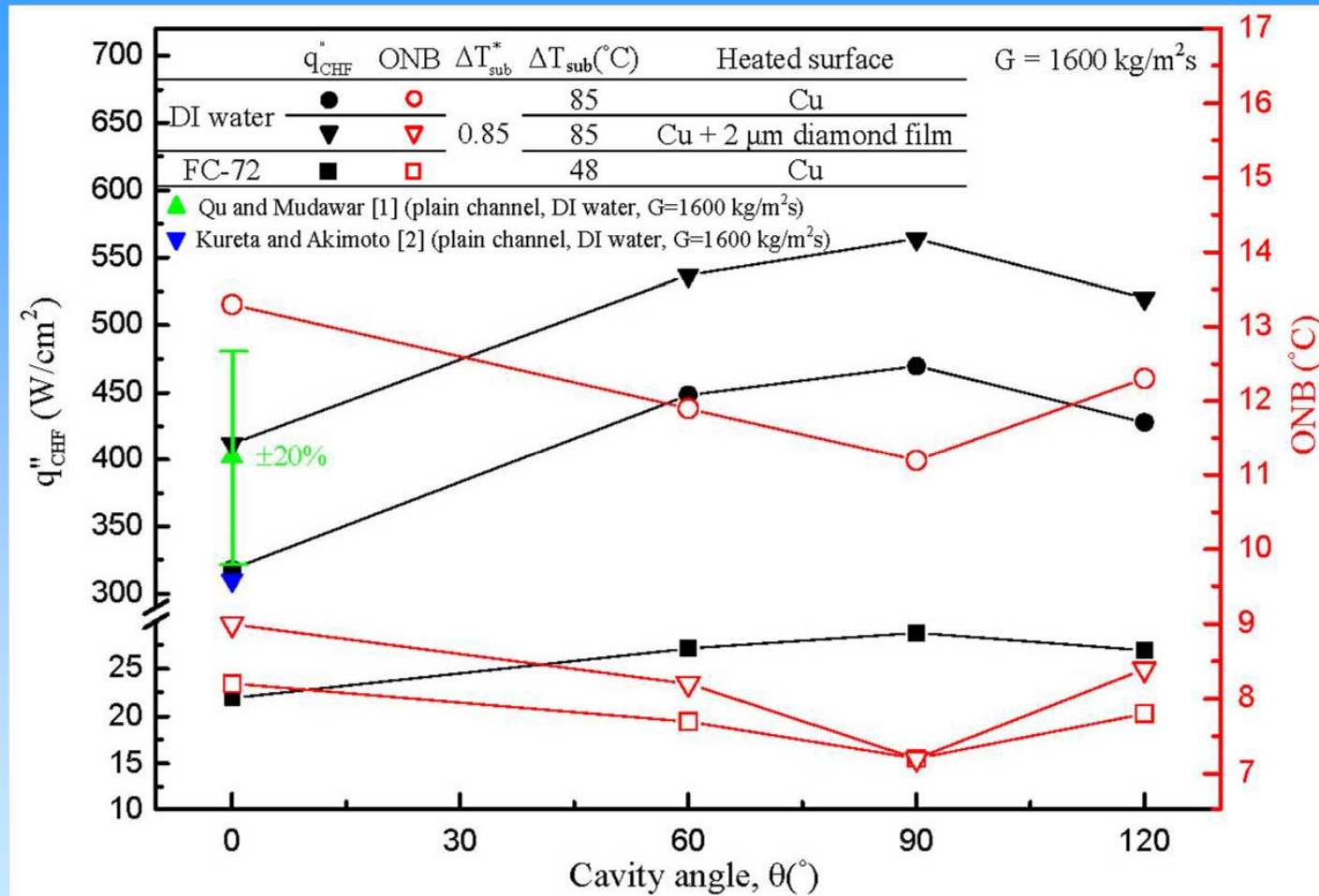
Schematic of (a) microchannel surface structure (b) cartridge heater

Flow Loop



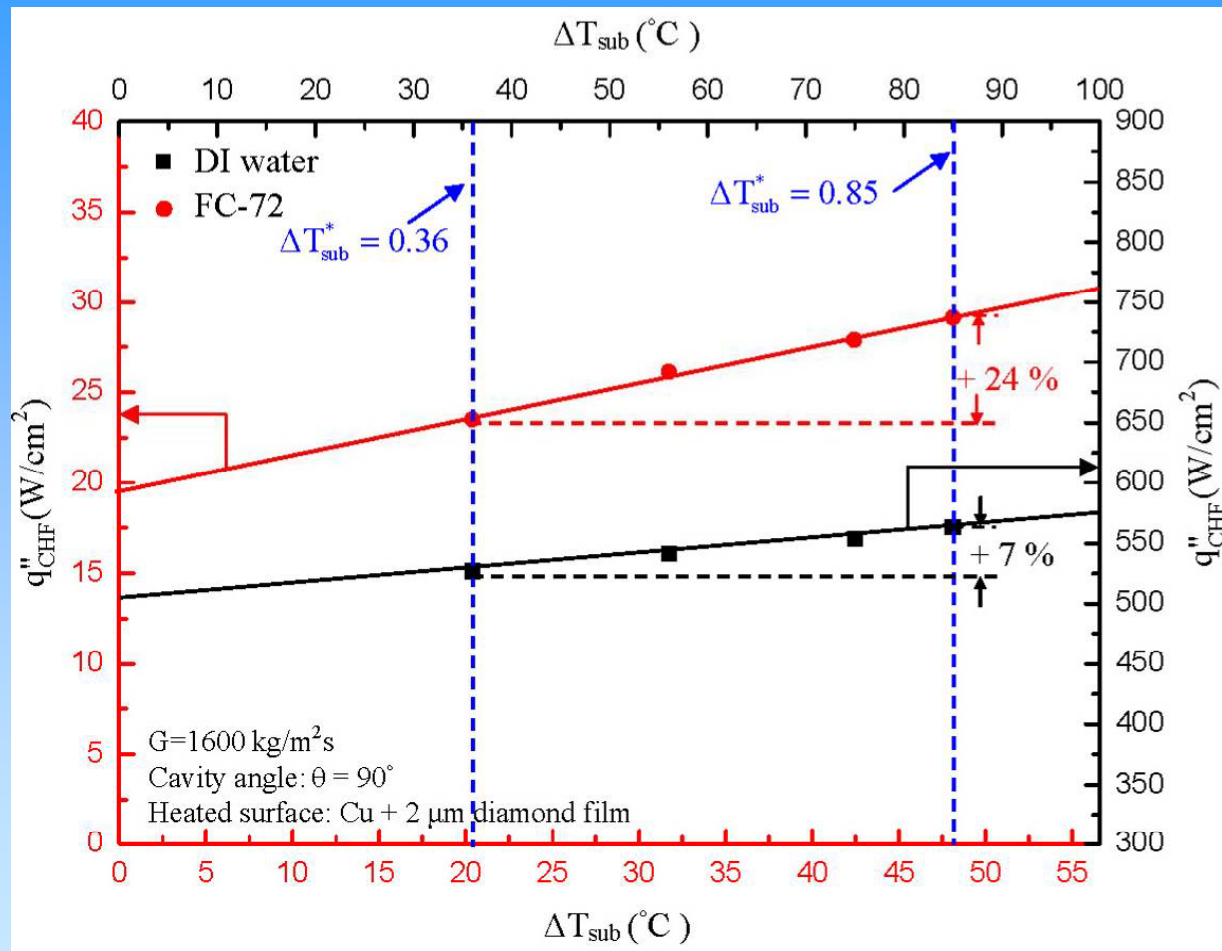
Test flow loop

Experimental Results



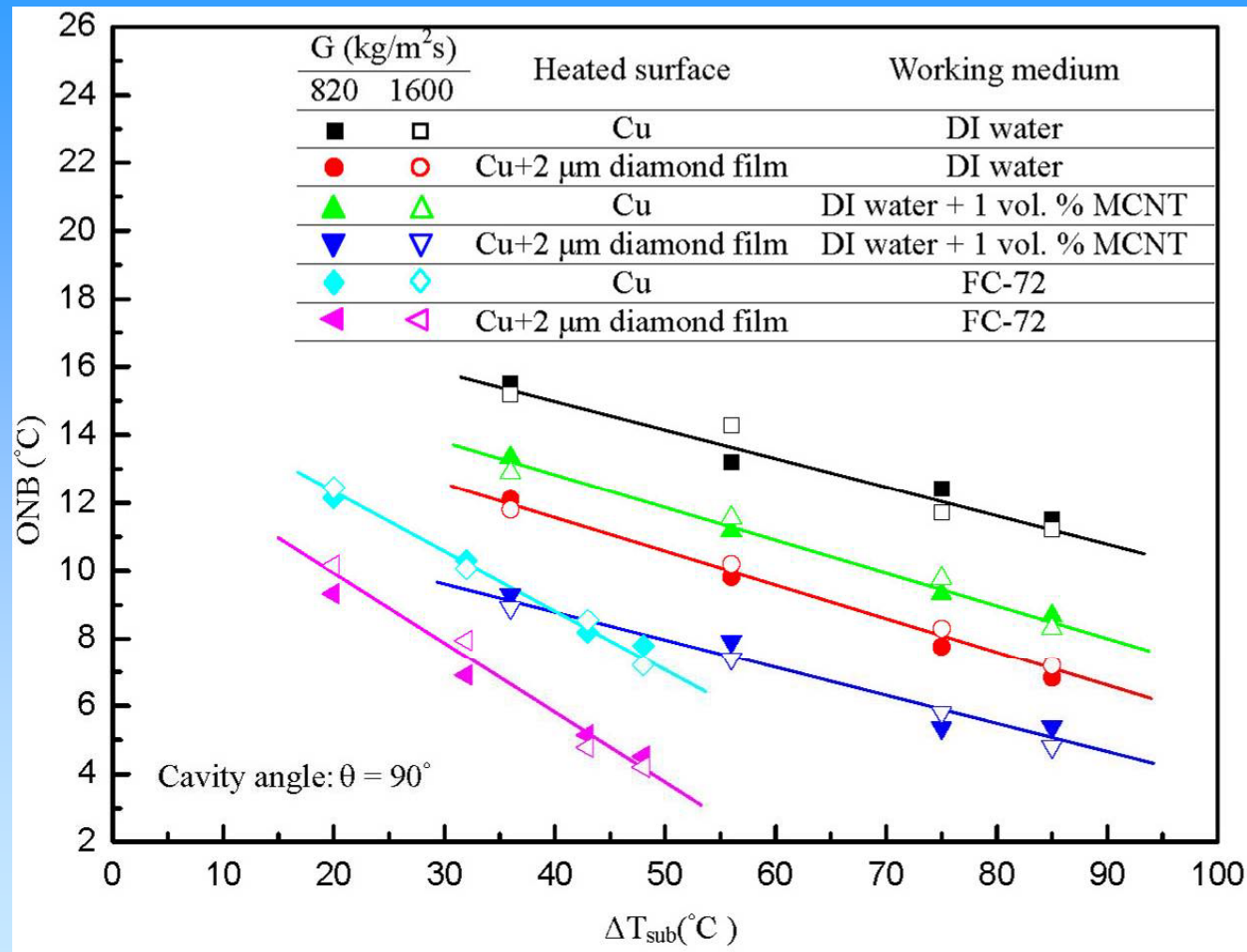
The cavity angle influence on q''_{CHF} and ONB

Experimental Results (continued)



Effect of subcooling on CHF for Water and FC-72

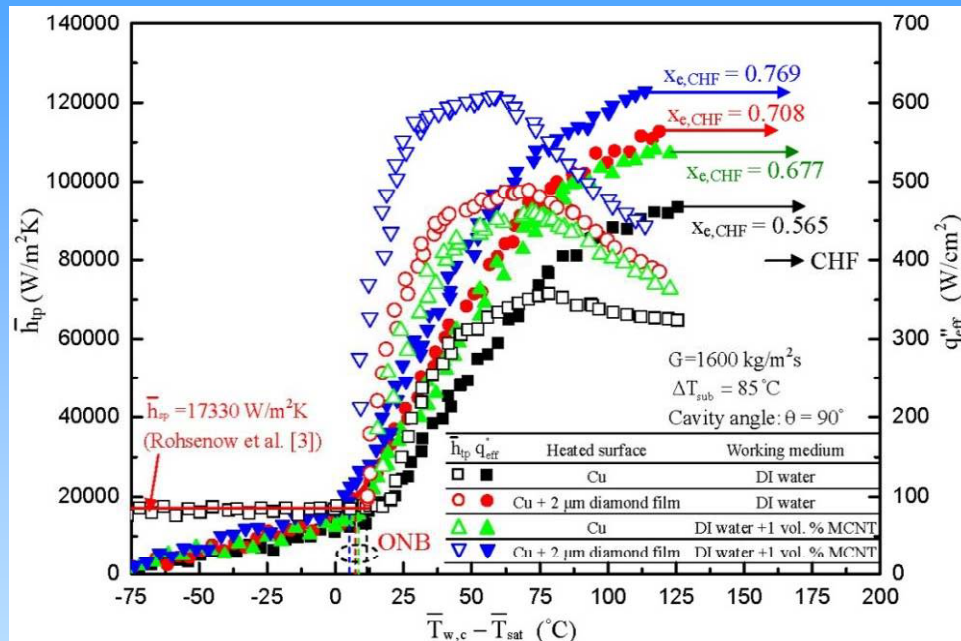
Experimental Results *(continued)*



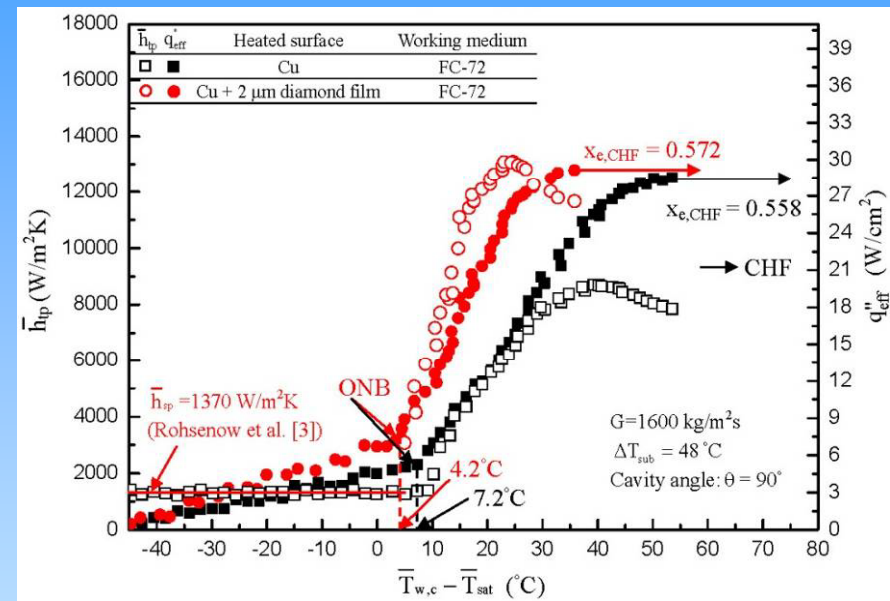
Effect of mass flux and subcooling on ONB for different test fluids

Experimental Results (continued)

(a)

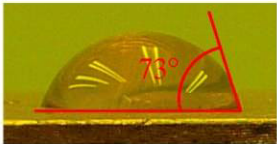
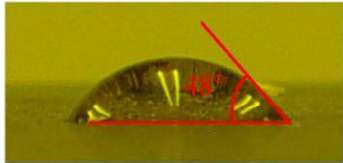
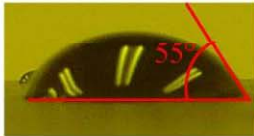
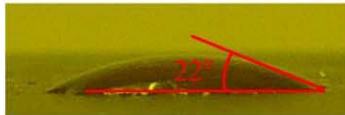
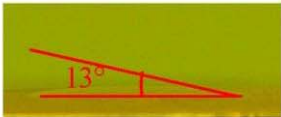
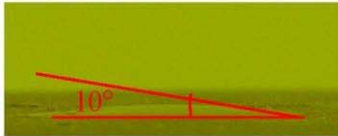


(b)



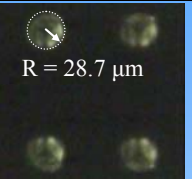
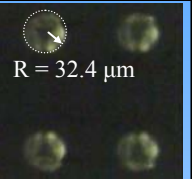
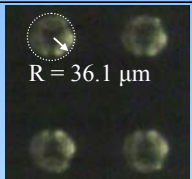
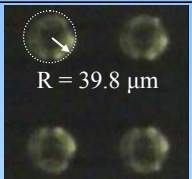
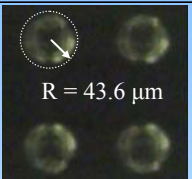
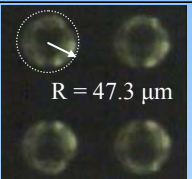
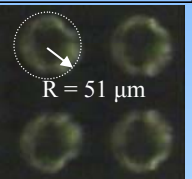
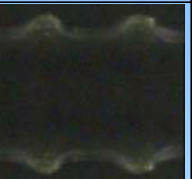
The boiling curves and average two-phase heat transfer coefficient of
(a) DI water with / without 1 vol. % MCNT (b) FC-72

Experimental Results *(continued)*

Working medium	Bottom surface of microchannel (heated surface)	
	Cu	Cu + 2 μm Diamond film
DI water		
DI water + 1 vol. % MCNT		
FC-72		

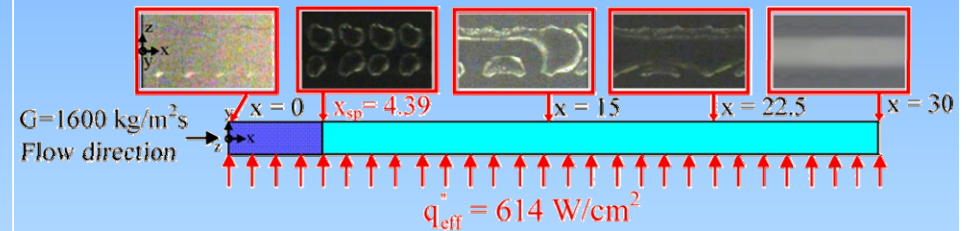
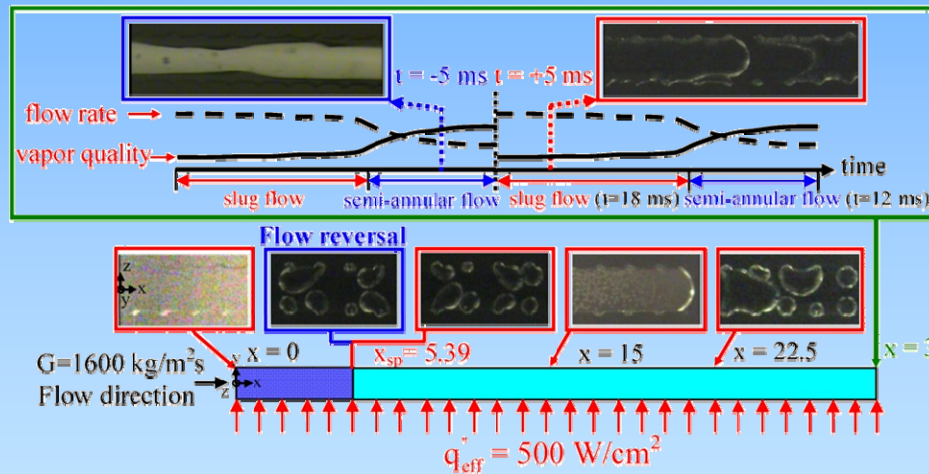
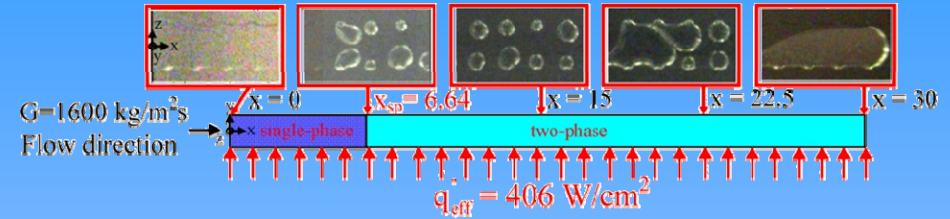
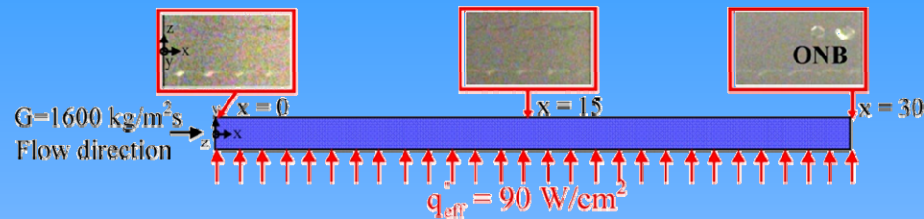
The contact angle (θ_c) of different heated surface and working medium

Experimental Results *(continued)*

t	t + 10 ms	t + 20 ms	t + 30 ms	t + 40 ms	t + 50 ms
	 R = 17.5 μm	 R = 21.3 μm	 R = 25 μm	 R = 28.7 μm	 R = 32.4 μm
t + 60 ms	t + 70 ms	t + 80 ms	t + 90 ms	t + 100 ms	t + 105 ms
 R = 36.1 μm	 R = 39.8 μm	 R = 43.6 μm	 R = 47.3 μm	 R = 51 μm	

A cycle of bubbles growing near the outlet at $q''_{\text{eff}} = 105 \text{ W/cm}^2$

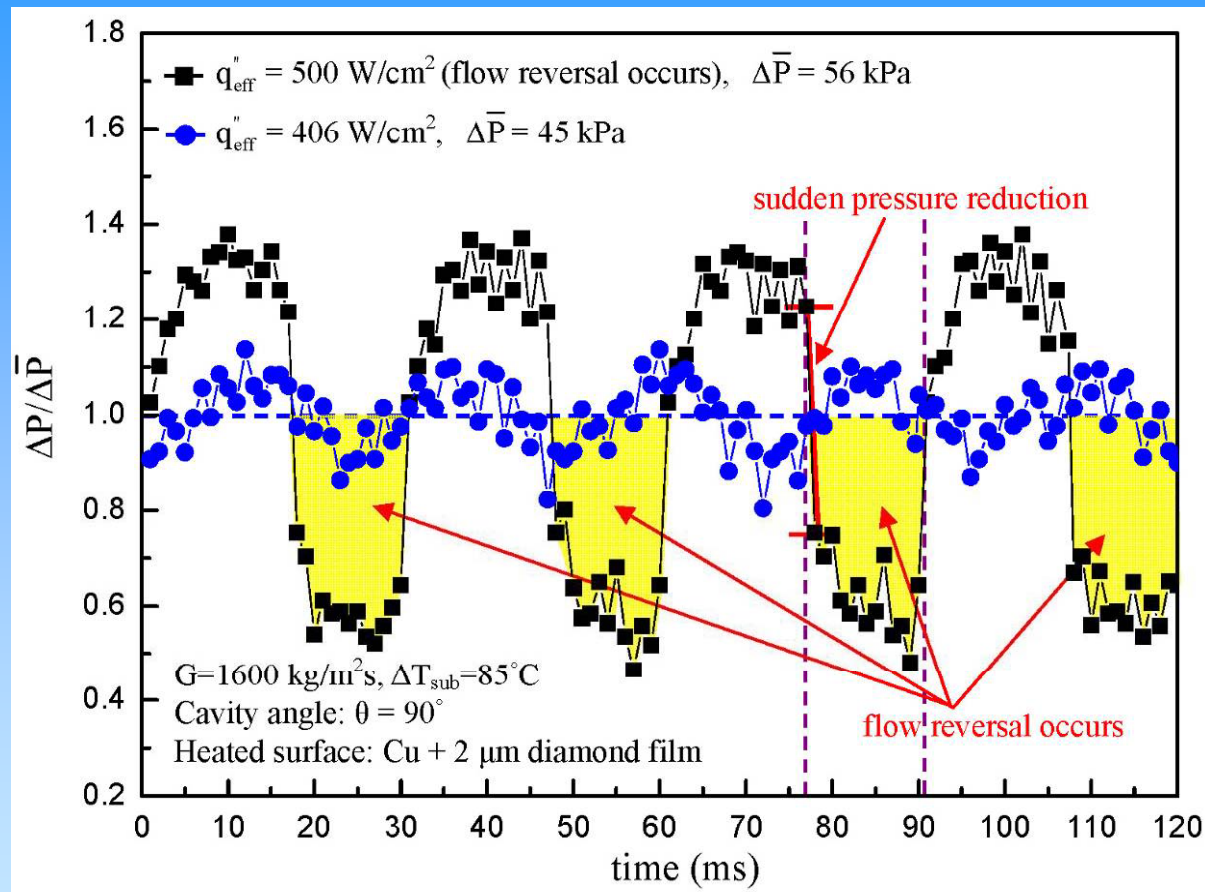
Experimental Results (continued)



Unit: mm

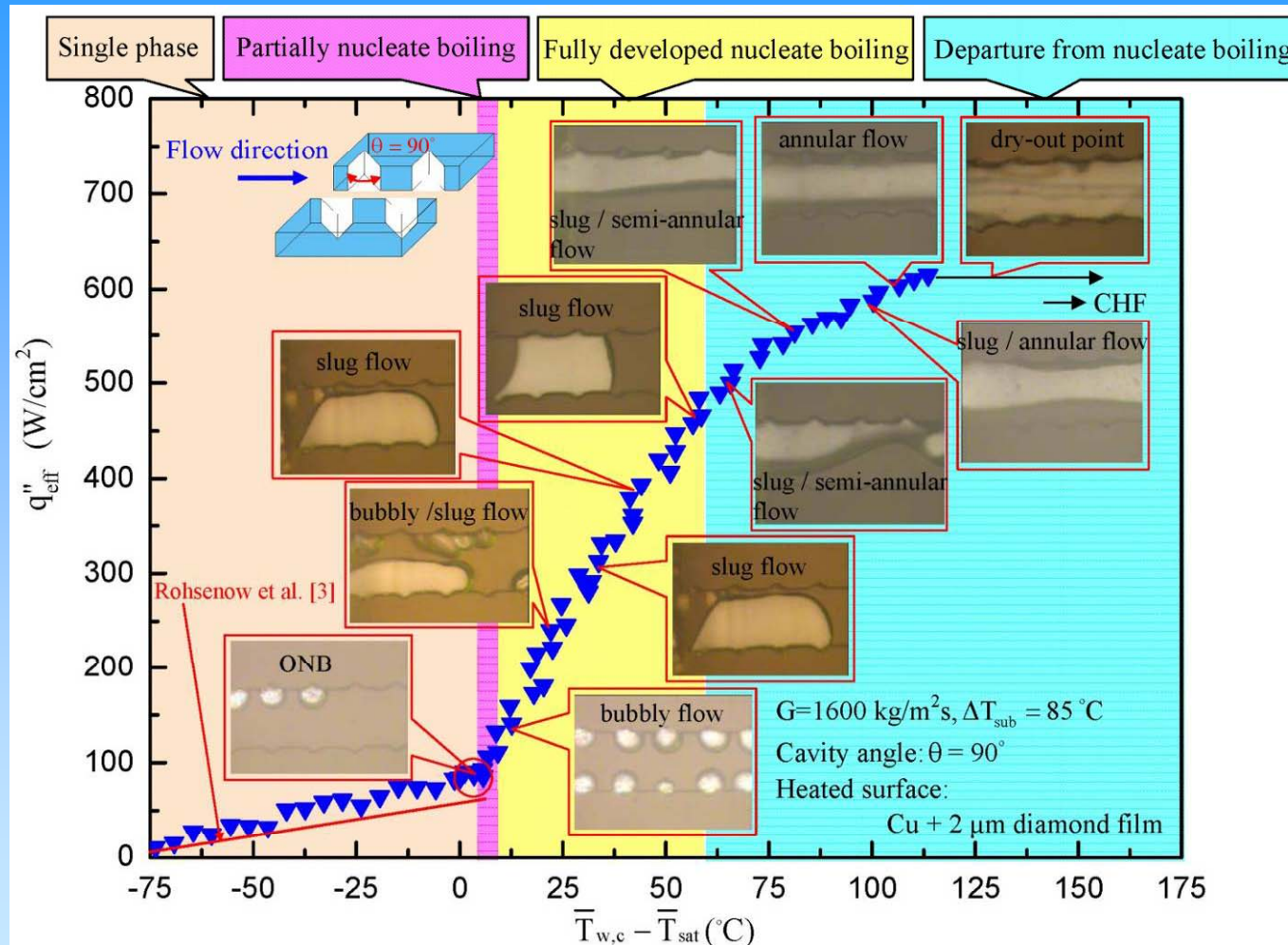
Flow patterns visualization from inlet to outlet at heat flux $q_{\text{eff}}'' = 90 \text{ W/cm}^2$, 406 W/cm^2 , 500 W/cm^2 and 614 W/cm^2 of DI water + 1 vol. % MCNT in the cavities ($\theta = 90^\circ$) channel

Experimental Results (continued)



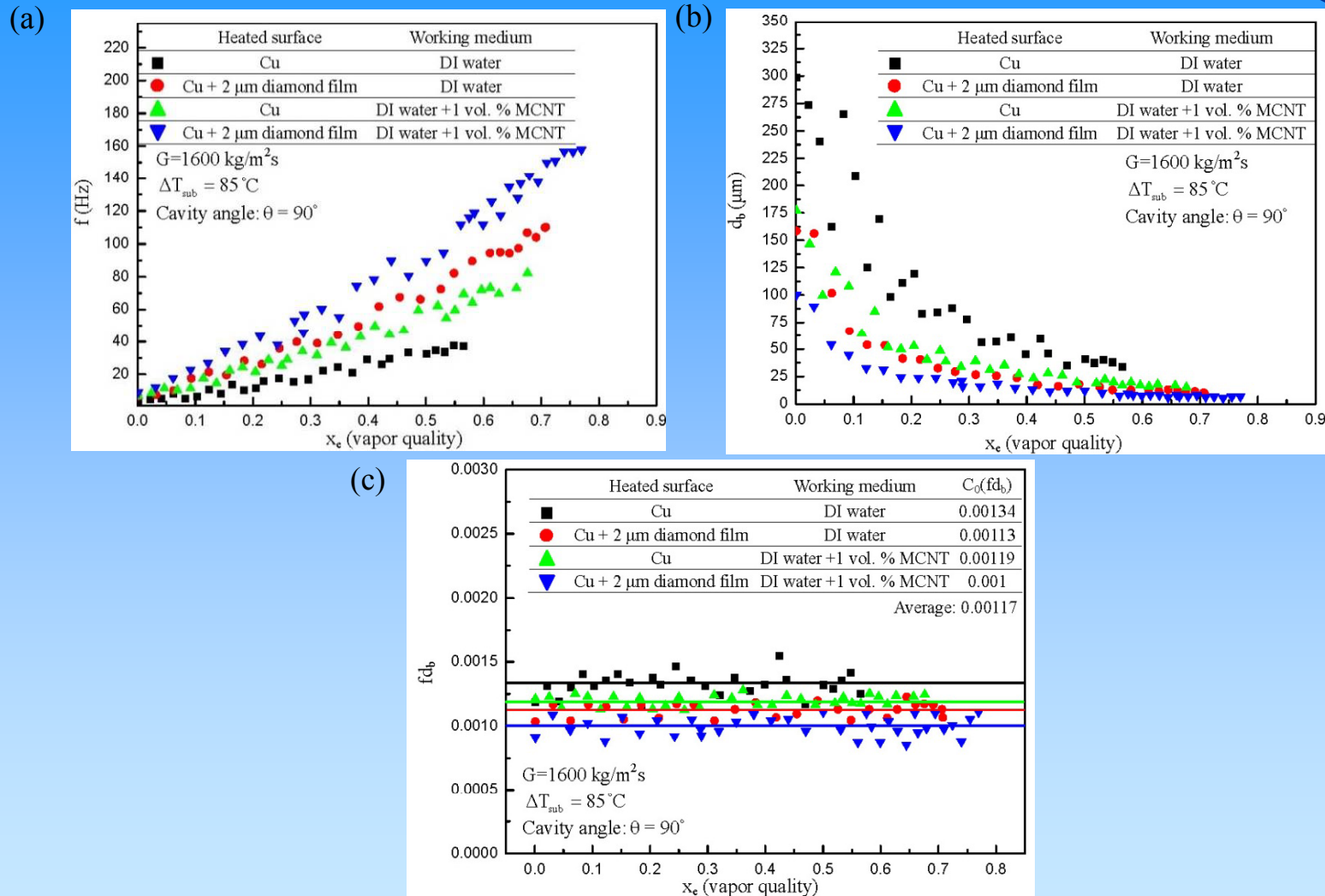
Pressure drop fluctuations of DI water + 1 vol. % MCNT with / without flow reversal

Experimental Results *(continued)*



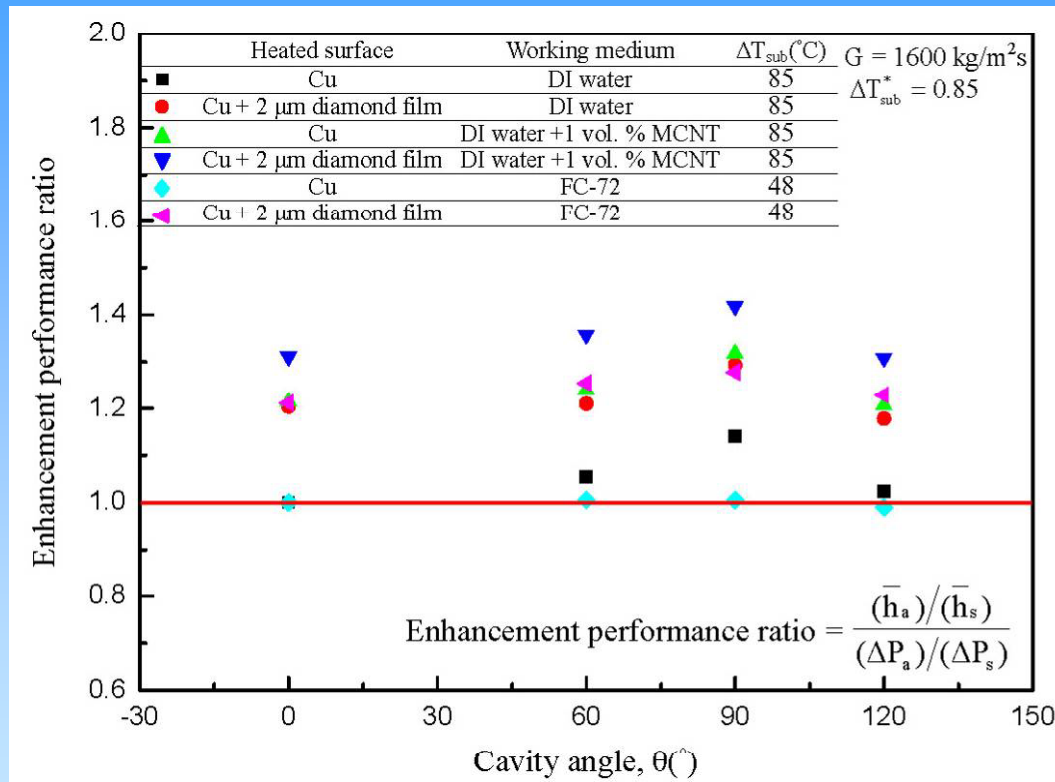
The boiling curve and corresponding flow patterns of DI water + 1 vol. % MCNT

Experimental Results *(continued)*



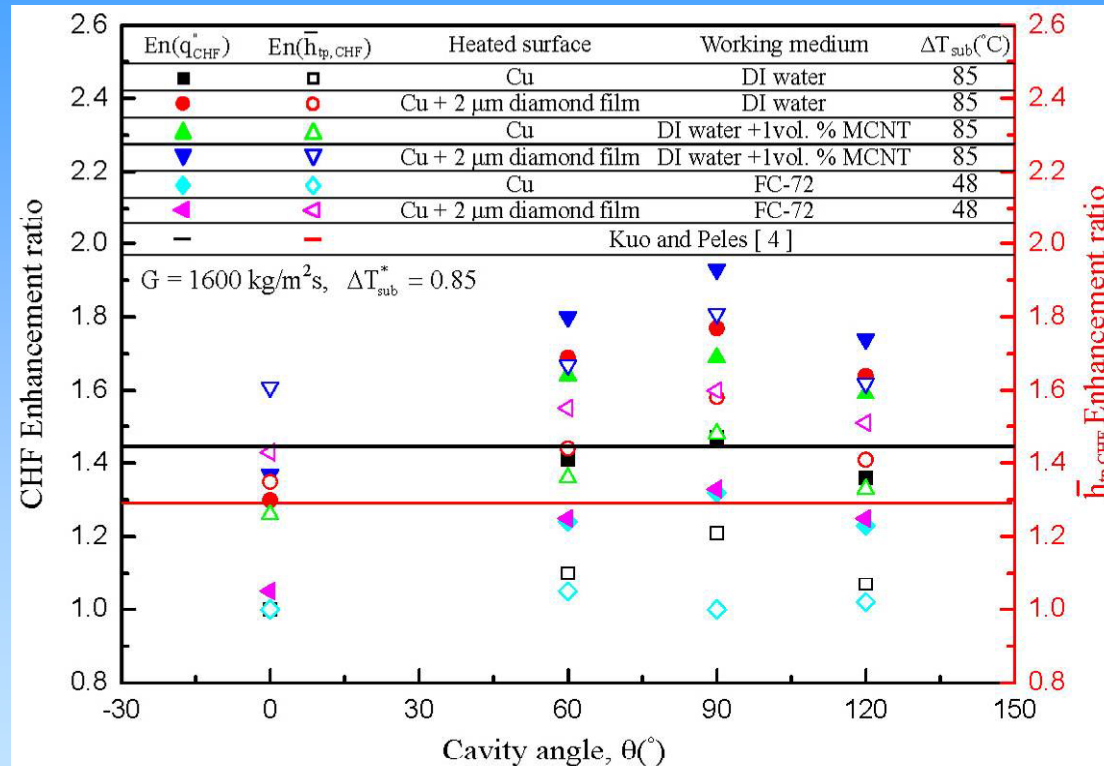
(a) bubble departure frequency and (b) the corresponding bubble departure diameter
(c) $fd_b = C_0$ at an active nucleation site near the outlet

Experimental Results *(continued)*



The enhancement performance ratio with different experimental conditions

Experimental Results *(continued)*



The comparison with present study and existing data in CHF and enhancement ratio

Conclusions



1. The effects of test fluids, heating / wall surface conditions, degree of subcooling, and mass velocity on ONB, $\bar{h}_{tp}$, q_{eff} and q_{CHF} were clearly noted.
2. DI water with *1 vol. % MCNT* particle additive in a Cu + 2 μm diamond film coating heating surface microchannel with internally structured surfaces had a superior thermal performance. It was found that the heat transfer enhancement ratio could be as high as *1.9* for a definite cavity angle.
3. An optimal cavity angle (θ) of 90° with *an enhancement performance ratio of 1.4* was found, as far as both heat transfer and pressure drop were concerned.
4. Following remark 1 and 2, a much higher heat flux was found at *614 W/cm²*.
5. The complex/combined effect of structured/thin film coating surface and nanofluids working medium on heat transfer enhancement in a flow boiling microchannel was found to be significant.

Salient References



1. W. Qu, and I. Mudawar, "Measurement and correlation of critical heat flux in two-phase micro-channel heat sinks," International Journal of Heat and Mass Transfer, Vol. 47, 2004, pp. 2045-2059.
2. M. Kureta, and H. Akimoto, "Critical Heat Flux Correlation for Subcooled Boiling Flow in Narrow Channels," Int'l. J. Heat Mass Transfer, Vol. 45, 2002, pp. 4107-4115.
3. W. M. Rohsenow, J. P. Hartnett, and E. N. Ganic, Handbook of Heat Transfer Fundamentals 2nd edn, New York: McGraw-Hill, 1985. pp. 7-94.
4. C. J. Kuo, and Y. Peles, "Local Measurement of Flow Boiling in Structured Surface Microchannels," Int. J. Heat and Mass Transfer, Vol. 50, 2007, pp.4513-4526.
5. S. -S. Hsieh, and C. Y. Lin, "Subcooled Convective Boiling in Structured Surface Microchannels," Journal of Micromechanics and Microengineering, Vol. 20, 2010, 015027(13pp).

Thanks for Your Attention !